

## High methane oxidation rates in ferruginous lake Matano

A. STURM<sup>1</sup>, S.A. CROWE<sup>2</sup>, C.A. JONES<sup>2</sup>, K.L. LESLIE<sup>1</sup>,  
D.E. CANFIELD<sup>2</sup>, S. NÓMOSATRYO<sup>3</sup>, A. MUCCI<sup>4</sup>  
AND D.A. FOWLE<sup>1</sup>

<sup>1</sup>Dept. of Geology, University of Kansas (arsturm@ku.edu)

<sup>2</sup>NordCEE, Syddansk Universitet, Odense Denmark

<sup>3</sup>Research Center for Limnology, Indonesian Institute of Sciences (LIPI), Cibinong-Bogor, Indonesia

<sup>4</sup>Earth and Planetary Sciences, McGill University, Montréal, Canada

Lake Matano is the 8<sup>th</sup> deepest lake on the planet and is the world's largest known ferruginous basin [1]. This ancient lake is persistently stratified, and beyond its high Fe content, it is characterized by extremely low SO<sub>4</sub><sup>2-</sup> and very high CH<sub>4</sub> concentrations. It has been proposed that CH<sub>4</sub> consumption in the lake occurs via a novel pathway in which CH<sub>4</sub> oxidation is coupled to the reduction of Fe and Mn (hydr)oxides [1]. To investigate the pathways of CH<sub>4</sub> consumption, we monitored methane oxidation rates with a <sup>14</sup>C-CH<sub>4</sub> tracer, both with and without the addition of a suite of electron acceptors including Fe and Mn (hydr)oxides. Our initial measurements yield volume specific rates as high as 0.8 μmol l<sup>-1</sup> d<sup>-1</sup>, comparable to modelled rates from C isotope and CH<sub>4</sub> concentration profiles [1]. Our measured rates, without added electron donor, are 7 orders of magnitude higher than those reported for the Cariaco Basin [2] and approximately 10 to 50 times higher than in Big Soda Lake, Nevada [3]. Considering the ultra-oligotrophic nature of Lake Matano, these are remarkably high rates. Electron acceptor addition experiments are in progress and these results will be discussed. Our results to date clearly show that CH<sub>4</sub> is an important component of the C cycle in Lake Matano and by extension ferruginous systems in general.

[1] Crowe *et al.* (2011) *Geobiology* **9**, 61–78. [2] Ward *et al.* (1987) *Nature* **327**, 226–229. [3] Iversen, Oremland & Klug (1987) *Limnol Oceanogr.* **32**, 804–814.

## Laboratory experiments and modeling of CO<sub>2</sub> dissolution in water for carbon sequestration

M. STUTE<sup>1,2\*</sup>, D. FERNANDEZ DE LA REGUERA<sup>1</sup>  
AND J.M. MATTER<sup>1</sup>

<sup>1</sup>Lamont-Doherty Earth Observatory, Palisades, NY 10964

<sup>2</sup>Barnard College, New York, NY 10027

(\*correspondence: martins@ldeo.columbia.edu)

The injection of CO<sub>2</sub> gas in the dissolved phase is an alternative to that of supercritical CO<sub>2</sub> if the depth of the formation is <800m, or where immediate solution trapping is desired because of safety concerns. The most efficient way to dissolve CO<sub>2</sub> in water is downhole in order to take advantage of the increased hydrostatic pressure. We conducted experiments in a 100m long 'well' set up in the staircase of a Manhattan building to study the dynamics of the dissolution process. CO<sub>2</sub> was added at the top of the well with a sparger and the dissolution process was monitored downstream by image processing technology.

The experimental results reveal that bubble size and density decrease along the flow path as expected. However, the rate of dissolution decreased along the flow path with bubbles dissolving rapidly initially and extremely slowly afterwards. As the bubbles decrease in size, they became harder to dissolve, due to effects of rigidity of the gas-liquid interface and the presence of low solubility gases in the water and gas. The degree of dissolution could be considerably enhanced by using a passive mixer or an active downhole submersible pump. The dissolution process was simulated using the Darcy-Weisbach equation and a one-dimensional multi-gas numerical gas exchange model. Besides CO<sub>2</sub>, common impurities such as N<sub>2</sub>, O<sub>2</sub>, noble gases, H<sub>2</sub>, H<sub>2</sub>S and gas tracers (SF<sub>6</sub> and SF<sub>5</sub>CF<sub>3</sub>) were included in the model. Extrapolation of the model parameters to real-world injection scenarios (e.g. the Carbfix pilot project in Iceland [1]) illuminate the role that the dissolved gas composition, the purity of the CO<sub>2</sub>, and temperature play in controlling the efficiency of CO<sub>2</sub> dissolution for storage in geologic formations.

[1] Gislason *et al.* (2010) *Int. J. Greenh. Gas Con.* **4**.